

# **Hydrodynamic Studies of Two-Phase Liquid-Liquid Slug Flow in Circular Microchannel with T-Junction**

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**Abstract.** Microreactors have a wide application, especially in heterogeneous reactions limited by mass and or heat transfer. In many chemical reactions, microreactors show good performance for obtaining a high yield, selectivity, and conversion up to 100%, which is not easy to realize using conventional reactors. The excellent performance of the microreactor is a result of the high stability of two phase flow, namely slug flow pattern. A comprehensive study of slug flow characteristics inside the microchannel is needed to have a good performance. For that reason, the present work focused on the study of slug flow characteristics and its stability by using a circular microtube with 0.5; 0.8, and 1 mm inside diameter, and the 2 liquid phase consisted of aquades-kerosene and aquades-ethyl acetate with aquades as a dispersed phase and kerosene or ethyl acetate as a continuous phase. These liquids represent two liquid mixtures with different physical and chemical properties, which significantly influence the formation of 2-phase flow patterns in a microtube. Variables used in the experiment were temperature, channel diameter, and volumetric flow rate. Observation results show that the slug flow pattern was found at the ratio of the volumetric flow rate of disperse phase to the continuous phase (*Qd/Qc*) is 1; 1.4; 1.8; and 2.2. The slug flow formed at a flow rate of 70 ml/h for both the dispersed phase and the continuous phase  $(Qd/Qc = 1)$ had the most stable droplet length and the distance of consecutive droplets. Increasing *Qd/Qc* ratio increases the droplet length formed, and in the range of discharge used, the change in inside tube diameter from 0.5 to 1 mm does not change the flow pattern model, but it affects the slug length.

*Keywords: microchannel, two-phase, flow pattern, stability, slug flow*

**Abstrak.** Teknologi *microreactor* memiliki aplikasi yang sangat luas, terutama pada reaksi heterogen yang dibatasi oleh perpindahan massa dan atau panas. Dalam banyak reaksi kimia, penggunaan *microreactor* telah mampu menghasilkan *yield* dan selektivitas yang tinggi dan bahkan konversi reaksi sebesar 100%, yang mana hasil ini sangat sulit dicapai dengan menggunakan reaktor konvensional. Kinerja unggul yang ditunjukkan oleh *microreactor* merupakan hasil dari pola aliran dengan kestabilan yang tinggi, yaitu pola aliran slug. Untuk dapat memanfaatkan kinerja unggul yang ditawarkan secara optimal, perlu dilakukan studi komprehensif tentang karakteristik pola aliran slug dalam *microchannel*. Karena itulah studi dalam penelitian ini memfokuskan pada pemahaman karakteristik pola aliran slug, serta kestabilannya. Percobaan dilakukan dengan menggunakan 2 fase liquid yang masing-masing bekerja sebagai fase terdispersi dan fase kontinu, yaitu air-kerosen dan air-etilasetat dengan sifat fisik dan kimia yang berbeda. Variabel suhu, diameter *channel*, laju alir liquid dipelajari pengaruhnya terhadap panjang slug dan jarak antar slug berdekatan yang terbentuk. Hasil observasi menyatakan bahwa pola aliran slug terbentuk pada rasio *Qd/Qc* sebesar 1; 1,4; 1,8; 2,2. Pola slug yang terbentuk pada debit 70 ml/jam baik untuk fase terdispersi maupun fase kontinu (pada *Qd/Qc* = 1) memiliki panjang droplet dan jarak antar droplet yang paling stabil. Peningkatan rasio *Qd/Qc* meningkatkan dimensi panjang droplet yang terbentuk, dan pada range debit yang digunakan perubahan diameter tube tidak merubah jenis pola aliran yang terbentuk, namun berpengaruh terhadap panjang slug.

*Kata kunci: microchannel, dua fase, pola aliran, kestabilan, aliran slug*

#### **INTRODUCTION**

Microreactor is a novel chemical reactor technology which has an excellent performance in carrying out a chemical reaction. This technology in many chemical synthesis applications mainly for heterogeneous systems has produced high yields and reaction conversions up to 100%. The heterogeneous reaction needs a large contact surface area to achieve optimal results. On the other hand, the conventional reactor can only provide a contact surface area (expressed as specific surface  $= A/V$ ) of 400 m2/m3, far below the specific surface that can be provided by a microreactor which is 40.000 m<sup>2</sup>/m<sup>3</sup> in the range channel diameter 10  $\mu$ m – 1mm.

Another excellent performance is shown concerning to the hazardous and toxic chemicals applications. In an industrial chemical processes, the product of chemical reaction that involves small volumes has been able to prevent



and avoid the risks posed by the use of hazardous and toxic materials in the process. The availability of a substantial specific surface in the miniaturization system of reactor has facilitated a mass/heat transfer process; therefore, the risk of work accidents such as explosions due to heat accumulation in a reactor can be prevented. The large specific surface in a microreactor has made the microreactor very suitable for applications in highly exothermic or endothermic processes that are limited by mass and or heat transfer.

The performance of a two-phase (liquid-liquid) microreactor is determined by the flow pattern type and the stability of flow formed within a channel. Among the flow patterns type that may develop in a channel, slug is the most stable flow pattern, has a regular velocity, uniform shape and distribution, with the slug length in several times of the inner diameter of the channel. Besides having high stability, slug flow pattern has a large specific surface area (A/V).

Several factors influence the formation of flow patterns in a microchannel, including the liquid viscosity and density, the wetting properties on the inner wall of channel, the contact angle, surface tension, the flow rate of the dispersed and continuous phase, the inner diameter of the channel, and the channel material. Previous researchers have carried out many studies on the effect of channel diameter on the flow pattern formed [1][2][3] using PTFE, PMMA, and glass channel [2][3][4][5]. The effect of liquid-liquid flow rate [4][6][7] with the different type of liquid used to represent the effect of liquid viscosity [2][3][4][8]. The droplet length and distance between successive droplets on slug flow has been investigated [4][5]. The studies are still limited to using PTFE, PMMA, and glass tube channel materials and several types of liquid phases as dispersed/continuous phases. Profound observation using various types of liquid, tube diameter, tube material, and flow rates will enrich the results of existing research. Understanding the flow pattern characteristics within a microchannel is necessary to get optimal results and it will be a significant consideration for determining a microchannel design. Therefore, this study aims to determine the effect of the flow rate of dispersed and continuous phase, the diameter of a microtube on flow pattern, the droplet length, and the distance between successive droplets on the slug flow. This study has focused on observing the flow pattern formed in a microchannel (without reaction) by using a variation of channel diameter (silicone) which has not been done in previous studies [1][2][4][9].

#### **EXPERIMENTAL METHODOLOGY**

The experiment was carried out with four variables: the flow rate of the dispersed and continuous phase, the components of liquid-liquid phase, temperature, and microchannel diameter. The flow rate and the components of liquid-liquid used in the experiment are shown in tables 1 and 2 below.





The experiment was performed at various temperatures of 28, 35, 40, 45, and 50 ℃, with channel diameters of 0.5; 0.8; and 1 mm, and 4.5 m channel long. The channel used in the experiment is tube silicone (circular microchannel).





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The immiscible liquid-liquid two-phase system was delivered by two low discharge syringe pumps, Yamamoto Giken YG-80 syringe pump that can deliver liquid phase in the range of  $0.1 - 99$  ml/hour, and Infusia SP7s syringe pump that can flow liquid phase in the range 0.010 – 999 ml/hour. The syringe pumps in this observation perform well in dispensing liquids with uniform and stable discharge. Observation of flow pattern was carried out with a 12 W LED light, and a digital camera (Sony A6000, 50 mm f1.8 lens and macro tube extension) connected to a computer, so that the flow pattern formed can easily be observed. Two computer programs applied are OBS and GIMP. The OBS program was to observe the flow patterns, and the GIMP was used to measure the dimensions of droplet length and droplet distance.







**FIGURE 2.** (a) The flow pattern observation scheme, (b) The measuring method of droplet length and droplet distance



The principle of the experiment is to make a contact with the two-phase liquid-liquid through T-junction (transparent material), therefore the formation of the flow pattern can be observed clearly. The experimental set-up is shown in the following Fig. 2.

#### **RESULTS AND DISCUSSION**

Liquid-liquid two-phase flow patterns in microtube can be classified into slug flow, droplet flow, thread flow, jet flow, and annular flow [9]. From these flow patterns, slug shows the stable flow characteristics and has excellent potential for developing process applications involving mass and or heat transfer, especially highly exothermic and endothermic processes. Therefore, this study focuses on observing the characteristics of slug flow pattern.

The slug flow formation is divided into the blocking, squeezing, and lag steps, as shown in Fig. 3 [7]. In the blocking step, the continuous and dispersed phases meet at the T-junction, and the dispersed phase tries to enter and penetrate to the main channel. The squeezing step can be described as the dispersed phase successfully entering the main channel, and the lag step is the step when droplets have formed.



(a) Blocking, (b) Squeezing, (c) Lag  $[7]$ 

Determination of flow rate is significant to get the right flow pattern. In this observation, slug flow formed when the dispersed and continuous phase flow rate ratio is 1; 1.4; 1.8, and 2.2 (Table 1 and 2).

#### **Liquid-Liquid Two-Phase Flow Pattern-Regime Slug Flow**

Slug flow is characterized by a fragmented flow pattern between the dispersed and the continuous phase, as shown in Fig. 4. The formation of slug begins at the meeting point of the dispersed and the continuous phase at T-junction. Fig. 4 shows the slug flow pattern on a microtube with 0.8 mm inside diameter, tube length (*Lt*) of 4.5 m with a meander channel configuration so that the microtube is like to be divided into four rows, with the 1<sup>st</sup> channel being the closest channel with the inlet section.





**FIGURE 4.**Slug flow pattern in aquades-kerosene,  $Q_{aq} = 25$  ml/hour,  $Q_{ke} = 25$  ml/hour,  $D_t = 0.8$  mm, T= 28 °C

The wetting property of liquid is a factor that determines the characteristics of the flow pattern formed. Interactions between the dispersed and the continuous phase with the inner surface of the tube wall determine the formation of a thin liquid film in a narrow space between the droplet and the inner tube wall.

In some previous works on the two-phase liquid-liquid system [1][6],the thin liquid film appeared in the observed system, whereas other studies [2][4][6] cannot detect the appearance of the liquid film within a slug flow pattern. The formation of the thin film is shown in the schematic Fig.5 (b).



**FIGURE 5.**(a) Droplet without film, (b) Droplet with film [9]

Experiments using aquades-ethyl acetate formed droplets with a film, whereas in the aquades-kerosene system, liquid droplets formed without a film (Fig. 5(a)). Ethyl acetate, as the continuous phase in the first liquid, pairs wetting the inner tube wall, while kerosene in the second liquid, pairs wetting the inner tube walls. In the aquades-kerosene system, it can be formed as a thin film but is not observed due to visual limitations. In many cases, particularly those involving mass and heat transfer, film formation is more advantageous than flow patterns without films because the appearance of these films increases the interfacial mass/heat transfer rates. S is the surface area of the droplet where the mass/heat transfer happens, and V is the enclosed droplet volume. In a flow pattern without film, the mass/heat transfer process occurs in the zone between two droplets, in an area between the heads and tails of successive droplets. However, in the flow pattern with film, a mass transfer does not only occur in that zone but also in the thin liquid film.

#### **Effect of Inner Diameter of Microtube to Liquid-Liquid Flow Pattern**

Two-phase flow patterns in aquades-kerosene and aquades-ethyl acetate with both dispersed and continuous phase flow rates of 25 ml/hour in different tube diameters are shown in Fig. 6. Fig. 6 shows that for a constant flow rate (25-25 ml/hour) at various tube diameters, it formed the same flow pattern, slug flow. Thus, at a constant flow rate, the different tube diameter in this experiment does not affect the flow pattern type but rather the droplet length formed. At a certain flow rate, changes in tube diameter can cause changes in the type of flow pattern from slug flow to annular flow. From the measurement of the droplets formed, in the aquades-kerosene system with a constant flow rate of 25- 25 ml/hour, the average length of droplets formed on a 0.5 mm diameter tube is 10.074 mm, tube diameter of 0.8 mm is 4.523 mm, and a tube with a diameter of 1 mm is 3,129 mm. At a constant flow rate, the tube diameter is getting larger, the shorter of the droplet length.



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**FIGURE 6.** (a), (c), (e) Flow pattern in aquades-kerosen; (b), (d), (f) Flow pattern in aquades-ethyl acetate

#### **The Stability of Slug Flow Pattern**

The channel used in this observation was arranged into four rows. Fig. 7-9 shows the droplet profile within the microtube.



**FIGURE 7.** Droplet dimension profile in aquades-kerosene U<sub>d</sub>-U<sub>C</sub>= 25-25 ml/hour (stable flow)





**FIGURE 8.** Droplet dimension profile in aquades-kerosene U<sub>d</sub>-U<sub>C</sub>= 35-25 ml/hour (unstable flow)

The difference in droplet length of about 1 mm from the average dimension indicates that the flow pattern within the microtube is stable. The more significant droplet length difference means the flow pattern's lower stability.



**FIGURE 9.** Droplet dimension profile in aquades-ethyl acetate *Ud*-*UC*=70-70ml/hour (stable flow)

The difference in droplet length, which is quite prominent in the microtube, is difficult to explain. The occurrence of this phenomenon may be caused by the pump's performance, which is not stable during pumping the two liquid phases, and another one is the coalescence phenomenon, mainly for tubes with huge length dimensions.

#### **The Effect of the Linear Velocity Ratio of Dispersed to Continuous Phase (***Ud/Uc***)**  to Droplet Length  $(L_b)$





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The larger *Ud/Uc* ratio was obtained by increasing the flow rate of aquades to the same flow rate of continuous phase increases in the droplet length dimensions in each microchannel. Table 4 indicates that an increase in two folds of the *Ud/Uc* ratio can increase the droplet length (*Lb*) by two times. This tendency is shown by the droplets on each microchannel. However, the effect of increasing the *Ud/Uc* ratio differs from the results shown in Table 5, i.e., an increase in the ratio up to 2 times can only increase 1.5 times the droplet length.

#### **Bubble Length Follows Garstecky Model**



**FIGURE 10.** The comparison of the experimental droplets length and Garstecky model for aquades-kerosene system, 1 mm inside diameter of the tube

The droplet length at the inlet section of the main channel has the dimension as shown in Fig. 10 and 11, Each for pairs of 2 liquid-liquid phases from aquades-kerosene and aquades-ethyl acetate. Garstecky, in the previous study, had formulated the correlation between the length of droplets (*Lb*) formed in the T-junction on the various ratio of dispersed phase to continuous phase (*Qd/Qc*) following the equation as below: with *Qd* = debit of the dispersed phase,  $Qc$  = debit of the continuous phase,  $W_{in}$  = channel diameter in the inlet section of the dispersed phase (aquades), and  $W =$  diameter of the main channel.





**FIGURE 11.** The comparison of the experimental droplets length and Garstecky model for aquades-ethyl acetate system, 1 mm inside diameter of the tube

When compared, the length of experimental droplet characteristic is appropriate to the proposed model by Garstecky, while the increase in *Qd/Qc* will be followed by the increase in the droplet length (*Lb*) with a linear trend. However, the value of *Lb* experiment and *Lb* based on this model was not the same. There are some possible factors: i.e., the Garstecky model has not considered the type of material channel, the liquid wettability to the inner wall of a microchannel, and the physical property such as liquid density and viscosity of the liquid that is used in the experiments.

#### **Dimensionless Numbers**

Capillary number, Reynold number, and Weber number are dimensionless numbers explaining the effect of three dominants force in a microchannel system; consist of inertial force, viscous force, and surface tension force. By comparing these dimensionless numbers, it will be known the influence of dominant force or less dominant in a slug flow formation of liquid-liquid system. The capillary number represents the ratio of the following forces [10]:

$$
Ca = \frac{viscousforce}{\text{surfacetensionforce}}\tag{1}
$$

The capillary number in this experiment is in the range of  $6.68 \times 10^{-5} - 8.719 \times 10^{-3}$  (Ca < 1). The value of capillary number below 1 indicates that surface tension force works more dominant than viscous force. Reynold number represents the ratio of inertial forces to viscous force as in the following equation [10]:

$$
Re = \frac{inertial force}{viscous force}
$$
 (2)

Reynold number experiment is in the range of  $3.2289 - 122.1798$  (Re  $> 1$ ). The value of Reynold number higher than 1 indicates that inertial force works more dominant than viscous force.

Weber number represents the ratio of inertial force to surface tension force as in the following equation [10]:

$$
We = \frac{inertial force}{\text{surface tension force}}
$$
\n(3)

Weber number in this experiment is  $1.062 \times 10^{-3} - 1.841 \times 10^{-1}$  (We < 1). Weber number below 1 indicates that surface tension force works more dominant than inertial force. Based on the value of Capillary number, Reynold number, and



Weber number, the influence of these forces on the liquid-liquid system of aquades-kerosene and aquades-ethyl acetate has the following order: surface tension force > inertial force > viscous force.

#### **CONCLUSION**

The slug flow hydrodynamic was investigated in a circular silicone microchannel with an inside diameter of less than 1 mm. The tube diameter in these experiments (0,5; 0,8; 1 mm) didn't affect the flow pattern type; it affected the droplet length and the distance of successive droplets. The increased channel diameter has brought on the lower droplet length. The slug flow pattern formed when the flow velocity ratio of the dispersed to continuous phase (*Ud/Uc)*= 1; 1,4; 1,8; 2,2. The greater value of *Ud/Uc* has resulted in the length of droplets within the microchannel. The various flow velocity use in these experiments consist of *Uc* = 25; 70 ml/hour, *Ud* = 25; 35; 45; 55; 70 ml/hour entirely formed slug flow pattern.

The higher temperature may influence the droplet lengths and the distances of successive droplets. The temperature has a correlation to the viscosity of liquid-liquid two-phase flow. Further, the droplet length showed the same trend as the length obtained by Garstecky model.

The dimensionless numbers consisting of Capillary Number, Reynold Number, and Weber Number are able to explain the influence of three dominant forces, i.e., surface tension force, inertial force and viscous force in a micro system.

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#### **Abstract**

*Microreactors have a wide application, especially in heterogeneous reactions limited by mass and or heat transfer. In many chemical reactions, microreactors show good performance for obtaining a high yield, selectivity, and conversion up to 100%, which is not easy to realize using conventional reactors. The excellent performance of the microreactor is a result of the high stability of two phase flow, namely slug flow pattern. A comprehensive study of slug flow characteristics inside the microchannel is needed to have a good performance. For that reason, the present work focused on the study of slug flow characteristics and its stability by using a circular microtube with 0.5; 0.8, and 1 mm inside diameter, and the 2-liquid phase consisted of water-kerosene and water-ethyl acetate with water as a dispersed phase and kerosene or ethyl acetate as a continuous phase. These liquids represent two liquid mixtures with different physical and chemical properties, which significantly influence the formation of 2-phase flow patterns in a microtube. Variables used in the experiment were temperature, channel diameter, and volumetric flow rate. Observation results show that the slug flow pattern was found at the ratio of the volumetric flow rate of disperse phase to the continuous phase*  $(Q_D/Q_C)$  *is 1; 1.4; 1.8; and 2.2. The slug flow formed at a flow rate of 70 ml/h for both the dispersed phase and the continuous phase (* $Q_D/Q_C$  $=$  1) had the most stable droplet length and the distance of consecutive droplets. Increasing  $Q_D/Q_C$  ratio increases the droplet length formed, and in the range of discharge used, the change in inside tube *diameter from 0.5 to 1 mm does not change the flow pattern model, but it affects the slug length.*

**Keywords:** microchannel, two-phase, flow pattern, stability, slug flow

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# **About STKSR 2022**

### **International Seminar on Chemical Engineering Soehadi Reksowardojo (STKSR) 2022**

International Seminar on Chemical Engineering Soehadi Reksowardojo (STKSR) is an annual seminar held by the Department of Chemical Engineering ITB in honour of Prof. Soehadi Reksowardojo's contribution to the early developments of chemical engineering higher education in Indonesia. This year STKSR 2022 will be held in Ambon, Indonesia and by virtual conference, starting from August  $9<sup>th</sup>$  to August  $10<sup>th</sup>$ , 2022. Bringing forward the theme "Building Indonesia Through the Development of Appropriate Technology For Archipelagic Country", we would like to invite scholars and practitioners from all around the world to contribute to these seminars.

Technological advances from the effects of globalization have provided changes for the better in human civilization, including in Indonesia. Unfortunately, this progress has not been felt evenly, especially among the Indonesian people who live on small islands. As we know, the distribution of electricity and clean water in Indonesia has not yet reached 100 percent. Development in the country is also still concentrated in areas with big cities so many people in remote areas are still left behind. The natural resources of each island are different and natural commodities are not sufficient so resources from other islands are needed. It is undeniable that the form of an archipelagic state makes access to the exchange of natural resources more limited. Indonesia as a maritime country also still has problems with a mindset that is focused on development on the mainland. Natural resources that are appropriate to be taken are sufficient to advance and even meet energy and material needs because technology has not yet been applied to process resources. Therefore, efforts are needed to develop appropriate technology to adapt to the geographical conditions of the country so that the sea acts as a land separator.

This seminar is purposed to campaign technological breakthroughs for archipelagic countries and become a form of ITB Chemical Engineering's contribution to national development. To find comprehensive ideas and formulations for the development of technology for the process of providing energy and resources in the archipelago, synergy is needed between stakeholders, including the community, academics, entrepreneurs, and the government. This synergy can be realized in a conference such as the 2022 STKSR as a forum to facilitate Indonesia's future interests in the development of technology in archipelagic countries.



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# **Speech of Rector Institut Teknologi Bandung**

<span id="page-17-0"></span>On behalf of Institut Teknologi Bandung, we welcome the honorably keynote speakers, invited speakers, speakers and all participant to the International Seminar on Chemical Engineering Soehadi Reksowardojo (STKSR) 2022. We also thanks Universitas Pattimura Ambon for the collaboration on this event, which brings theme of "Building Indonesia through the Development of Appropriate Technology for Archipelagic Country".

As mentioned in the seminar title, Prof. Ir. Soehadi Reksowardojo is a prominent figure in ITB, who brought the concept of "Tri-Soko-Guru" for higher education. The "Tri-Soko-Guru" means three main pillars, consist of education, research, and industry affiliation. The concept then nowadays evolves into "Tri Dharma Perguruan Tinggi" of education, research, and community service. In accordance with ITB's mission to guide the change that able to improve welfare of Indonesian and the world, The Tri Dharma Perguruan Tinggi bridge innovation on the research to real implementation on the industry and society. As we know, the innovation is the key aspect to avoid the middle-income trap. The researches as a core of innovation therefore should explore uniqueness of Indonesia and each country to develop a competitiveness.

Archipelagic country, such as Indonesia, has advantages as well as different set of technology challenges compare to the continent countries. With abundant of natural resources at sea, we need a specific technology to process them into a useful goods. In example, microalgae as a source of food and oil for biodiesel, is a competence agent for  $CO<sub>2</sub>$  reduction in atmosphere. The oil extraction process from the microalgae should overcome high water content, differentiate the technology from the other oil sources extraction such as palm oil. This seminar is a way to disseminate the research's results and to collaborate among the researcher, thus able to increase readiness level of the technology.

We believe this seminar will be fulfilled with fruitful discussions and innovative technologies that suitable for the archipelagic countries. Finally, we express our highest gratitude and appreciation to our sponsors, collaborators, committees, and participants who greatly contribute to the success of the STKSR 2022. Hopefully, this event brings the best results for all.

**Prof. Reini Wirahadikusumah, Ph.D.**

**Rector of ITB**



# **Conference Topics**

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# **Keynote Speakers**

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## **Dr. Ir. I.G.B. Ngurah Makertihartha**

Catalyst Expert & Scientist Department of Chemical Engineering Institut Teknologi Bandung

### **Prof. Dr. Iftekar Abubakar Karimi**

Department of Chemical and Biomolecular Engineering National University of Singapore





**Ir. Jaya Wahono**

Chief Executive Officer Clean Power Indonesia

### **Dr. Eng. Muhammad Aziz**

Associate Professor of Energy and Prosses Integration Engineering The University of Tokyo





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### **Dr. Dadan Kusdiana**

Director General NRE&EC Ministry of Energy and Mineral Resources

# **Prof. Guoqing Guan**

Institute of Regional Innovation Hirosaki University





# **Seminar Schedule**

#### <span id="page-21-0"></span>**RUNDOWN DAY 1**

# **Tuesday, 9th August 2022**

#### **PLENARY SESSION DAY 1 (08.00-13.45)**





#### **RUNDOWN DAY 2**

# **Wednesday, 10th August 2022**







#### **PARALLEL SESSION DAY ONE (13.45-17.30, Masella Building)**

**Note:** Paper code that is written in bold are for paper that will be presented offline. The session in room 5 and 6 will be held fully online





#### **PARALLEL SESSION DAY TWO (08.30-13.30, Masella Building)**

**Note**: Paper code that is written in bold are for paper that will be presented offline. The session in room 5 and 6 will be held fully online



# **List of Accepted Abstract**

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#### **Topic 2:** Food Engineering and Technology (FET)

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#### **Topic 3:** Bioprocess Engineering (BPE)







**Topic 4:** Chemurgy and Bio-based Materials (CBM)



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**Topic 5:** Advanced Science and Materials (ASM)



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#### **Topic 6:** Separation Technology (ST)











#### **Topic 7:** Process Simulation (PS)









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#### **Topic 8:** Industrial Application (IA)













**Topic 10:** Chemical Engineering Education (CEE)





#### **List of Poster**

